

TECHNICAL BULLETIN

MODEL: "HFL" Flash Tank

TB No. S5050

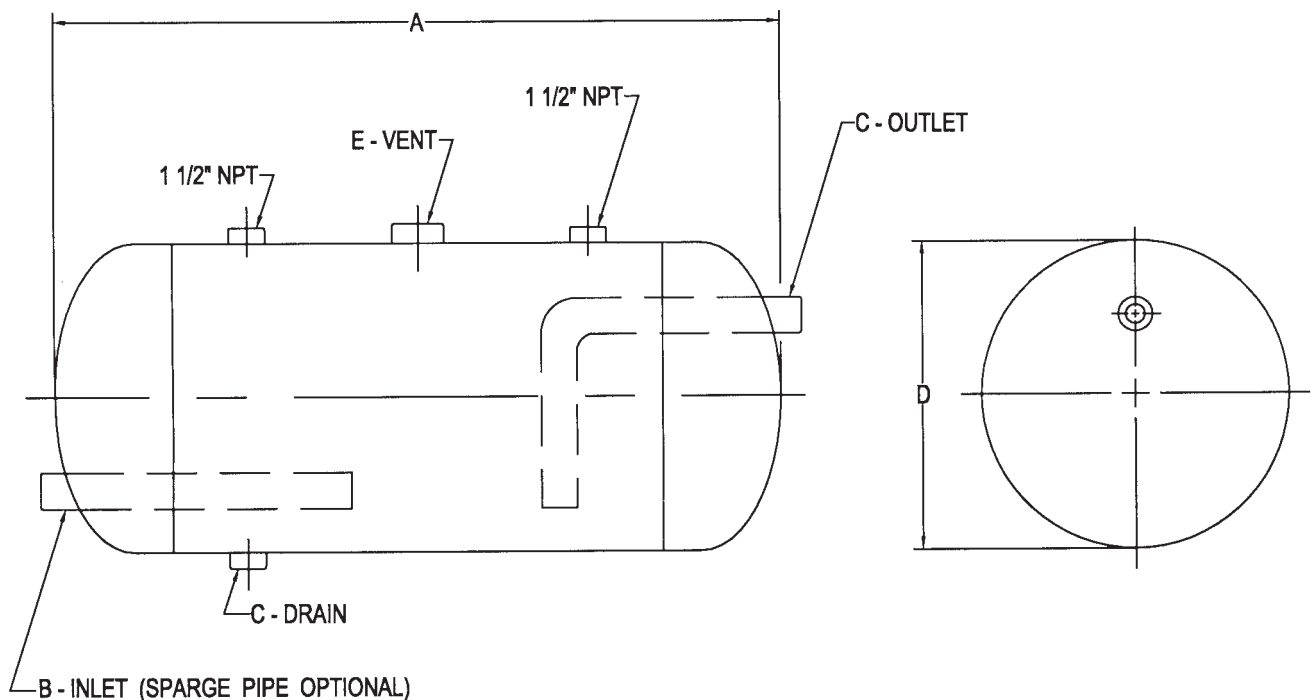
Date 1-01

DESCRIPTION

The "HFL" flash tanks are designed for systems that require flashing of high pressure condensate into steam for low pressure heating supply mains, and to reduce and cool low pressure steam before it is returned to the boiler, condensate receiver, or discharged into sewer.

STANDARDS

These vessels are designed in accordance with ASME Code Section VIII, Div. 1 and can be ASME Code Stamped for 150 psig steam service. Higher pressure upon request



DIMENSIONS AND WEIGHTS

MODEL NUMBER	GAL./ CAP.	A	B NPT	C NPT	D O. DIA.	E NPT	WEIGHT LBS.	SPARGE PIPE OPTION
HFL - 10	13	39"	1"	1 1/2"	10 3/4"	2"	80	1 1/2" x 18" with 20 - 3/8 holes
HFL - 12	18	39"	1"	1 1/2"	12 3/4"	2"	95	
HFL - 14	24	39"	1"	1 1/2"	14"	2"	110	
HFL - 16	30	38"	1 1/2"	1 1/2"	16"	2 1/2"	125	
HFL - 18	48	48"	2"	1 1/2"	18"	2 1/2"	170	
HFL - 24	80	46"	2"	2"	24"	3"	215	2" x 24" with 32 - 3/8 holes
HFL - 30	125	48"	2 1/2"	2"	30"	3"	285	
HFL - 36	180	48"	3"	2"	36"	3"	340	

*NOTE: SPARGE PIPE IS AVAILABLE AS OPTIONAL EQUIPMENT. LARGER CAPACITIES, WORKING PRESSURES AND FITTING AVAILABLE.

MODEL: "FL5" FLASH TANK

TB No. S5000

Date 1-01

SAMPLE SPECIFICATION

Flash Recovery Vessel shall be mild steel construction ASME Code Stamped for 150 psig steam service with ANSI 150# RF flanges. Connections for a pressure gauge and a Safety Relief Valve shall be provided in the shell.

INSTALLATION

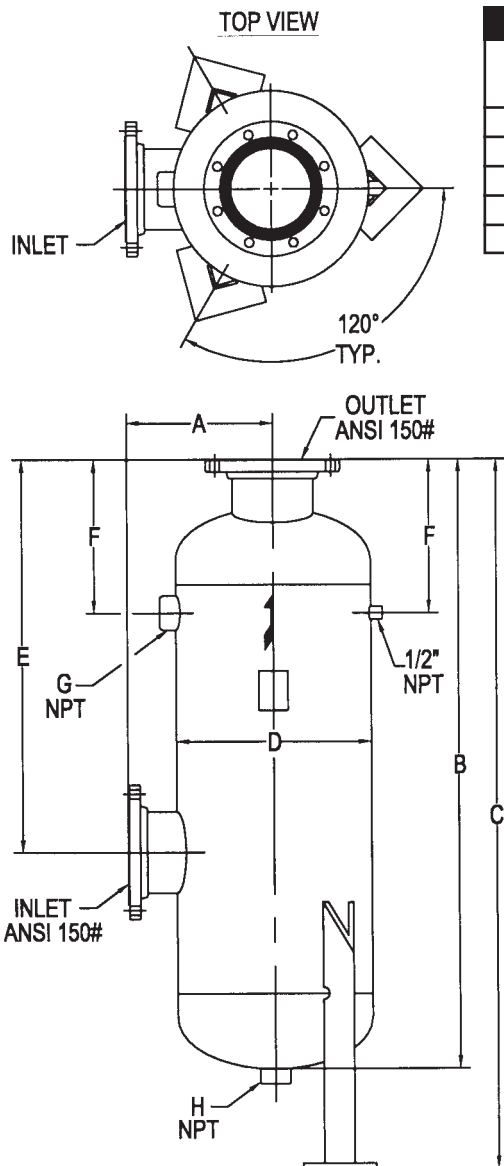
The vessel should be installed with the flash steam outlet at the top as shown. Each size vessel incorporates a 1/2" NPT connection for the fitting of a pressure gauge. If a Safety Relief Valve is required, it should be fitted in the NPT connection provide in the side of the shell. For drainage, a properly sized float type steam trap must be connected to the condensate outlet at the bottom of the vessel.

STANDARDS

These vessels are designed in accordance with ASME Code Section VIII, Div. 1 and can be ASME Code Stamped for 150 psig steam service.

HOW TO SIZE

Fig. 1 shows the proportions by weight of flash steam formed from condensate with various pressure drops. From Fig. 1, find the weight of flash per unit weight of condensate. Multiply this by the maximum condensing rate to get the maximum weight of flash steam expected from the flash vessel. Select the appropriate size flash vessel from Fig. 2 by finding the area within which both the condensate rate and the flash steam weight fit.



DIMENSIONS									
SIZE	INLET/OUTLET	A	B	C	D	E	F	G	H
4"	1 1/2"	6"	36"	45"	4 1/2"	24"	8"	3/4"	3/4"
6"	2 1/2"	7"	38 1/2"	47"	6 5/8"	22 1/2"	9"	3/4"	1 1/2"
8"	4"	8"	39 1/2"	48"	8 5/8"	25 7/8"	9 1/2"	3/4"	2"
12"	5"	10"	41 3/8"	49 1/2"	12 3/4"	26 7/8"	11 1/2"	1 1/2"	3"
16"	6"	12"	49 3/4"	58"	16"	32"	12 1/2"	2"	3"

FIG. 1
PROPORTION OF
FLASH STEAM

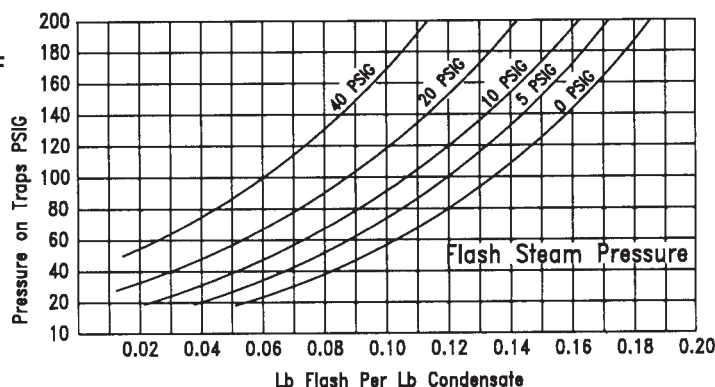
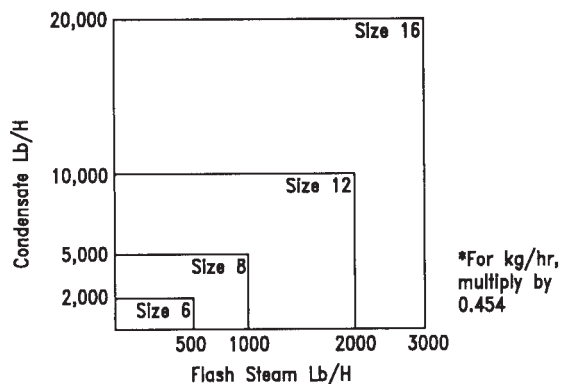


FIG. 2
RECOVERY
VESSEL
CAPACITIES



*For kg/hr,
multiply by
0.454